Availability of public goods shapes the evolution of competing metabolic strategies

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Availability of public goods shapes the evolution of competing metabolic strategies

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Tradeoffs provide a rationale for the outcome of natural selection. A prominent example is the negative correlation between the growth rate and the biomass yield in unicellular organisms. This tradeoff leads to a dilemma, where the optimization of growth rate is advantageous for an individual, whereas the optimization of the biomass yield would be advantageous for a population. High-rate strategies are observed in a broad variety of organisms such as Escherichia coli, yeast, and cancer cells. Growth in suspension cultures favors fast-growing organisms, whereas spatial structure is of importance for the evolution of high-yield strategies. Despite this realization, experimental methods to directly select for increased yield are lacking. We here show that the serial propagation of a microbial population in a water-in-oil emulsion allows selection of strains with increased biomass yield. The propagation in emulsion creates a spatially structured environment where the growth-limiting substrate is privatized for populations founded by individual cells. Experimental evolution of several isogenic Lactococcus lactis strains demonstrated the existence of a tradeoff between growth rate and biomass yield as an apparent Pareto front. The underlying mutations altered glucose transport and led to major shifts between homofermentative and heterofermentative metabolism, accounting for the changes in metabolic efficiency. The results demonstrated the impact of privatizing a public good on the evolutionary outcome between competing metabolic strategies. The presented approach allows the investigation of fundamental questions in biology such as the evolution of cooperation, cell–cell interactions, and the relationships between environmental and metabolic constraints.

metabolic engineering | group selection | r/K selection | droplets | microbial diversity

Although the existence of tradeoffs in evolution seems to be undisputable, experimental evidence obtained under controlled conditions is scarce. Several examples failed to show tradeoffs (1–4), whereas others could find them (5, 6) or found general but not universal tradeoffs (7, 8). A tradeoff between growth rate and growth yield in microbes (9–11) has direct implications for experiments carried out in liquid cultures. This is especially of importance during prolonged cultivations such as laboratory evolution experiments. In suspension, fast-growing variants outcompete slower growing ones at the cost of biomass yield (5). The yield versus rate optimization is governed by a dilemma where fast growth is advantageous from the perspective of an individual cell, whereas slow growth, and therefore high yield, is advantageous from the perspective of a population. This dilemma is consistent with a concept termed the tragedy of the commons (12). It is well described that spatial structure is essential for the selection of high-yield strategies (13–15). The yield/rate tradeoff of microbial growth has been linked to metabolic strategies (11) such as the switch between respiration and fermentation in yeast (9). It is suggested that the underlying cause of this tradeoff is based on thermodynamic principles, which describe that the rate of an isolated metabolic reaction is driven by free-energy dissipation and hence is negatively correlated with the product yield (9). However, it remains unclear if this is also valid for growth of an organism where near-equilibrium thermodynamics do not necessarily apply. Several studies that tried to address the yield/rate tradeoff experimentally failed. Luckinbill compared strains that were either adapted by serial propagation during exponential growth or in stationary phase (16). Velicer and Lenski compared strains that evolved in either carbon-limited chemostat cultures or in batch cultures (2). Both studies assumed that during the exponential phase of a batch culture, there was excess of substrate and therefore fast growing mutants should become dominant, whereas in either stationary phase or a carbon-limited chemostat, nutrients are limited and mutants that use their substrate efficiently should become dominant. We think that the reason why these and other studies (4, 6) failed to identify a yield/rate tradeoff over the course of experimental evolution is that in all cases the experiments were carried out in suspension cultures. In such an unstructured environment resources are a public good and accessible to every individual. In the case of batch cultures, this will select for the fastest growing organism, whereas in the case of a chemostat, selection will favor mutants with a higher affinity to the limiting substrate (17).

In theory, the selection of cells with increased metabolic efficiency but potentially slower growth rates is only possible if there is no or only limited substrate competition between fast and slow growing cells. We showed that such criteria are met in an emulsion-based serial propagation protocol, which favored the selection of strains with an increased number of offspring but decreased growth rates. The mechanism underlying those phenotypic changes was a shift in metabolic efficiency caused by altered glucose transport.

Results

Selection During Serial Compartmentalization in Emulsion. To select mutants with an increased number of offspring rather than increased growth rate, competition between individual cells needs to be eliminated through e.g., compartmentalization of single


The authors declare no conflict of interest.

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Data deposition: Sequence reads have been deposited in the NCBI Sequence Read Archive (SRA), www.ncbi.nlm.nih.gov/sra (accession nos. SRR917852 and SRS385748).

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This article contains information online at www.pnas.org/lookup/suppl/doi:10.1073/pnas.1308523110/-/DCSupplemental.
Exploring the Yield/Rate Tradeoff During Serial Propagation in Emulsion. We then explored the yield/rate tradeoff in isogenic L. lactis cells through serial propagation of chemically mutagenized populations in emulsions. Bacteria were allowed to grow for 2 days in the individual droplets and after 22 propagation cycles 88 individual colonies from two independent cultures were isolated. Growth rates and the maximum optical densities, which were used as a proxy for the total biomass yield, were determined for the individual cultures. One of the 88 strains (designated HB60) showed an 25% increase in maximal optical density, a 26% increase in culture dry weight, a 47% decrease in growth rate (MG1363 $\mu = 0.79 \text{ h}^{-1}$, HB60 $\mu = 0.42 \text{ h}^{-1}$), a 38% decrease in cell volume (MG1363 = 3.97 $\mu$m$^3$, HB60 = 2.45 $\mu$m$^3$), and a 71% increase in the total number of cells per culture volume (Fig. 2 and SI Appendix, Fig. S2). The results furthermore showed that after 22 propagation steps, most isolates cluster closely together in the yield/rate plot (Fig. 2A), whereas after 28 and 31 transfers multiple populations with more distinct properties arise. Interestingly also variants arise that seem to be slower and have a lower optical density compared with other variants in the same population. This indicates that optical density measurements might not always be representative for the number of offspring or that selection is also influenced by properties such as survival in stationary phase. Although we only characterized one strain of the above experiment in depth we are confident that the enrichment of strain HB60 was no coincidence. This was evident from the continuation of the original propagation experiment (Fig. 2) but also from the proof-of-principle experiment (Fig. 1) and the invasion of HB60 in the wild-type strain with its lactate dehydrogenase (ldh) negative derivative. In the ldh mutant, the glycolytic flux is diverted from lactate toward acetate (Fig. 1C), which results in a higher ATP- and biomass yield but also a decreased growth rate (Fig. 1D). Our experiments showed that in suspension, the wild-type strain rapidly won the competition, whereas in emulsion, the slow growing ldh mutant became dominant (Fig. 1E). This demonstrates a fundamental difference in selection pressure between the two culturing systems.

Fig. 1. Serial propagation in suspension leads to the selection of mutants with increased growth rates (A). If droplets in emulsions are initially occupied with a single cell, mutants with a higher number of offspring will be able to grow to a higher cell density compared with the wild-type strain even if such mutants grow slower. If the emulsion is subsequently broken, diluted, and used to inoculate a new emulsion, one can enrich for strains with a higher number of offspring will have increased competition (Fig. 1B). By repeating such a transfer regime in emulsion, cells with an increased number of offspring will be selected (Fig. 1A and B). We validated this concept by competing a Lactococcus lactis strain with its lactate dehydrogenase (ldh) negative derivative. In the ldh mutant, the glycolytic flux is diverted from lactate toward acetate (Fig. 1C), which results in a higher ATP- and biomass yield but also a decreased growth rate (Fig. 1D). Our experiments showed that in suspension, the wild-type strain rapidly won the competition, whereas in emulsion, the slow growing ldh mutant became dominant (Fig. 1E). This demonstrates a fundamental difference in selection pressure between the two culturing systems.

cells. Additionally, the number of compartments has to be high to guarantee a large enough population size for selection to act on. We reasoned that these criteria are met in a water-in-oil (w/o) emulsion. The water phase consists of the growth medium of an organism while the droplets in the emulsion are surrounded by an oil phase that prevents diffusion of molecules between individual droplets (Fig. 1). Following a Poisson distribution (e.g., $\lambda = 0.1$), droplets can be inoculated with single cells that are the founders of new populations in each droplet (SI Appendix, Fig. S1). Given sufficient time, populations in each droplet can grow to the maximum carrying capacity of the given medium. At the end of the incubation, the fraction of mutants that are producing a higher number of offspring will have increased compared with the fraction of these mutants at the time of inoculation. After breaking the emulsion, the cells are pooled in the medium (water) phase. At this stage, cells can be enumerated, diluted, and used again for the inoculation of the following emulsion. By repeating such a transfer regime in emulsion, cells with an increased number of offspring will be selected (Fig. 1A and B). We validated this concept by competing a Lactococcus lactis strain with its lactate dehydrogenase (ldh) negative derivative. In the ldh mutant, the glycolytic flux is diverted from lactate toward acetate (Fig. 1C), which results in a higher ATP- and biomass yield but also a decreased growth rate (Fig. 1D). Our experiments showed that in suspension, the wild-type strain rapidly won the competition, whereas in emulsion, the slow growing ldh mutant became dominant (Fig. 1E). This demonstrates a fundamental difference in selection pressure between the two culturing systems.

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propagation of this culture in emulsion up to 28 (and/or decreased growth rates. The data also indicate that several clusters resulted in an increased fraction of strains with increased optical densities slower but reaches a higher cell density.

Metabolic Shift and Its Effect on Growth Yield and Growth Rate. The metabolic shift of the wild-type M1363 (black line) and isolate HB60, which grows strongly selective pressure of the culturing conditions on the populations from a low frequency (SI Appendix, Fig. S3). Taken together, the results are consistent with the idea that propagation in a compartmentalized environment would enrich for strains with an increased number of offspring. In the case of HB60, the increased number of offspring also coincides with an increased biomass yield and a decreased growth rate indicating a yield/rate tradeoff.

Major Metabolic Shift Caused Decreased Growth Rate but Increased Biomass Yield. Whereas the wild-type strain MG1363 produced mainly lactate as a metabolic end product, HB60 produced mainly acetate, formate, and ethanol (SI Appendix, Figs. S4). This represents a metabolic shift in fermentation products, which is a major determinant of the ATP yield per glucose molecule (metabolic efficiency). We subsequently tested the stability of this metabolic strategy during cell propagation in suspension. Three independently propagated cultures of HB60 showed that within 90 generations, the cultures were dominated again by fast growing variants (designated HB61, HB62, and HB63) with decreased yield, increased cell size, and lactate as the major metabolic end product (Fig. 3 and SI Appendix, Fig. S5). These results suggest a strong selective pressure of the culturing conditions on the metabolic shift and its effect on growth yield and growth rate.

Altered Glucose Transport Caused the Metabolic Shift. Genome resequencing of strain HB60 revealed a point mutation in ptnC (SI Appendix, Fig. S6), which encodes a component of the main glucose transport system of L. lactis. This phosphoenolpyruvate:phosphotransferase system (designated PTSMan because of its initial description as a mannose transporter) is the only high-affinity glucose transporter in this strain (K_m = 13 μM), whereas the other glucose transport systems, the glucose permease glcU and the PTS_Glc system (a PTS that is also known to transport cellobiose) have K_m values of 2.4 mM and 8.7 mM, respectively (18). The sugar concentration at the beginning of our batch cultures was 5 mM and therefore mutations in the high-affinity system are expected to have the largest effects on glucose transport in our selection medium. In L. lactis, the acidification rate is a measure of the glycolytic flux. We found that HB60 had a 41% decreased acidification rate compared with the wild type, whereas the three fast growing revertants HB61, HB62, and HB63 showed acidification rates that were, respectively, 27%, 45%, and 32% increased relative to the wild type (SI Appendix, Fig. S7). Alterations from a high to a low glycolytic flux lead to a shift from the lactate toward the acetate branch and vice versa, changing the ATP yield and explaining the observed alterations in biomass yields. Genome resequencing of fast growing revertant strains showed that strain HB61 and HB63 have the transposable element IS905 inserted in the promoter region of PTSMan, encoding ptnABCD. Additionally HB63 has IS905 also inserted upstream of the glucose permease glcU. IS905 contains an outward facing perfect –35 promoter element at its 3′ end. Upon transposition upstream of ptnABCD and glcU new consensus promoter sequences are formed with –10 promoter elements located in the appropriate spacing on the integration locus (SI Appendix, Figs. S8 and S9). An increase in transcription levels upon transposition of IS905 into other promoter regions of MG1363 has been described earlier (19, 20). The transpositions of IS905 can therefore explain the enhanced acidification rate phenotype of the revertant strains HB61 and HB63.

**Fast Growth Rates Were Strongly Linked to Lactate Production.** A comparison of all strains evolved in this study, including two mutant strains that were deficient in two glucose transport systems, revealed a significant negative correlation of growth rate and growth yield over all 22 strains (adjusted R^2 = 0.71, P < 0.001). A scatter plot of yield/rate trajectories during selection in emulsion (dotted black line) and in suspension (solid lines). L. lactis MG1363 (black dot) was propagated in emulsion, which led to the isolation of HB60 (red dot). Subsequently HB60 was propagated in suspension for 160 generations. The solid arrows show the trajectories followed by three individual cultures of HB60 after 60, 100, and 160 generation in suspension. The dots after 100 generations are from single colonies isolated from the respective cultures, designated HB61 (green), HB62 (blue), and HB63 (turquoise). Gray dots show other isogenic isolates of MG1363 (SI Appendix, Fig. S10). SEs are indicated (n = 11).
Discussion

The described work is relevant to several related concepts in evolutionary biology. Serial propagation in emulsion describes the periodic isolation and propagation of single individuals, which underlies the concept of group selection (22) and has previously been described with the haystack model (23). Each droplet in the emulsion would be the equivalent of a haystack in the periodic isolation and propagation of single individuals, whereas the relevance of group selection in nature was the subject of intense discussions (23, 24), we show that periodic isolation does lead to a fundamentally different evolutionary outcome if compared with populations with continuously interacting individuals.

The described yield/rate tradeoff is also necessary to understand the mechanism of r/K selection. In r/K selection theory, high growth rate (r) is beneficial at low population densities and high food availability. However, at high population densities, close to the carrying capacity (K), food is scarce and its economic use is favored (25). It is assumed that selection acts reciprocally on the parameters r and K of a population (26). The demonstrated yield/rate tradeoff suggests the fundamental nature of this prerequisite for r/K selection theory. However, we would like to note that in our system faster growing cells not only waste energy by producing lactate, they also spent longer periods under starvation conditions in stationary phase. The latter by itself potentially favors the selection of slow growing cells in the presented propagation system.

The evolution of restrained growth phenotypes was shown earlier in systems that combined limited dispersal and/or spatial structure with ecological feedback. Examples include experiments with a community of three competitors that are engaged in a nontransitive (rock–paper–scissors) relationship (27) or the evolution of bacterial cross-feeding, which is costly for the individual but benefits the community (28). Compared with those studies, we show that the evolution of restraint is also possible without ecological feedback if the selection regime directly aims at an increased number of offspring. Another example for the evolution of restraint is described for bacteriophages of Escherichia coli. Two phage strategies lead to a “tragedy of the commons” by either being fast in infecting host bacteria but with low productivity when alone or vice versa. The selection of either phage strategy is determined by spatial restrictions in migration patterns (29, 30). The presented approach permits the variation of cells/phages per droplet in the emulsion, which will allow the investigation of interactions in microbial communities, which hitherto could not be addressed because of the limited number of compartments available in standard culturing techniques.

Cooperative traits often relate to extracellular molecules that confer a benefit to the total population but are a burden for the producing cell. Because of this burden the expression of extracellular proteases in lactococci (31, 32), invertase expression in yeast (33), or siderophore production in the pathogen Pseudomonas aeruginosa (34) are described as unstable. Such cooperative traits are expected to behave fundamentally differently in a suspension compared with an emulsion-based culturing system. The described approach should therefore open new possibilities for the investigation of the evolution of cooperation as well as facilitate the selection of strains with increased production levels of industrially relevant biomolecules such as extracellular substrate degrading enzymes.

Other industrial applications of the described selection procedure include the increase of biomass yield or the reduction of unwanted metabolic side products that are associated with fast growth such as acetate production in E. coli cultures (35) or ethanol production in respiring yeast (36). Furthermore, metabolic engineering strategies are increasingly based on genome-scale metabolic models, in particular through flux balance analysis (FBA). Such stoichiometric models optimize the molar yield of metabolic networks, which is discrepant with experimentally evolved organisms that are mostly optimized for growth rate (37). The selection of cells with optimized biomass yield therefore provides a direct correspondence between model predictions and evolutionary outcomes, allowing in silico design in metabolic engineering (38).

Our selection scheme for microbial biomass yield is similar to compartmentalized self-replication (CSR), a technique used...
Materials and Methods

6. Novák M, Pfeiffer T, Lenski RE, Sauer U, Bonhoeffer S (2006) Experimental tests for an evolutionary trade-off between growth rate and yield in the compartmentalization of cells. Moreover, we demonstrated how the yield/rate tradeoff affects the evolutionary outcome in structured and unstructured environments. The evolutionary solution of walking along a yield/rate Pareto front through alterations in sugar uptake systems is intriguingly simple.

Materials and Methods

Strains and Media. L. lactis MG1363 (43) and derivatives were used throughout this study. Experiments were carried out at 30 °C in a chemically defined medium (CDM) (44), which was supplemented with 5 mM glucose (GCDM) with the exception of the competition experiment of NZ9000 and N92010 (proof-of-principle experiment) where 25 mM glucose was added. Bacterial plating was done on the rich medium M17 (Oxoid) supplemented with 25 mM glucose (GM17).

1. 1H,1H,2H,2H-perfluorooctanol (Alfa Aesar) and frequent light shaking of the tube over a period of up to 15 min. This resulted in the separation of an oil and a water phase. After the separation of the two phases 700 μL of GCDM was added and 900 μL of medium with the bacterial cells was transferred to a sterile tube. The number of bacteria in this solution was then determined using a Coulter Counter (Beckman-Coulter). Subsequently, the cells were diluted in GCDM to give a concentration of 2 x 10^5 cells per milliliter and a new emulsion was prepared as described. This process was repeated serially for up to 31 times. Throughout the experiments, stock solutions of cells from broken emulsions supplemented with 15% (vol/vol) glycerol were prepared and stored at −80 °C in regular intervals.

Isolation of Strains with Increased Final Optical Density. The serial propagation of mutagenized L. lactis MG1363 in emulsion was carried out in duplicate. After 22 propagation steps, dilutions from each broken emulsion were prepared and plated on LB agar. The single colonies from each propagated emulsion were isolated and transferred to a 96-well microplate prepared and plated on GM17. A total of 44 single colonies from each well were propagated in fourfold into a 384-well microplate filled with 200 μL GCDM. After growth for 2–3 h, these cultures were propagated in fourfold into a 384-well microplate filled with 100 μL of GCDM. Cells in the original 96-well plate were allowed to grow for 20–24 h, and subsequently glycerol was added to each well to a final concentration of 15% (vol/vol) upon which the plate was frozen at −80 °C. The inoculated 384-well microplate was placed in a microplate reader and the optical densities at 600 nm were recorded for each well every 10 min for 48 h.

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Propagation in Emulsion. Three hundred microliters of a freshly inoculated L. lactis culture was used to make an emulsion by shaking it for 3–4 min with 250 μL water-based mixture of 30% vol/vol surfactant (2% Perfluoroctane 1H,1H,2H,2H-perfluorooctanol (Alfa Aesar) and frequent light shaking of the tube). Shaking was carried out at 2,200–2,300 rpm in capped 10-mL tubes (Greiner Bio-One; 164161). After shaking an emulsion separated in the tube from the surplus of oil within a few minutes and 650 μL of the oil phase was removed from the bottom of the tube. Cells were allowed to grow in emulsion at 30 °C for 1 or 2 d and subsequently the emulsion was broken. The breaking was done by adding 300 μL of 1H,1H,2H,2H-perfluorooctanol (Alfa Aesar) and frequent light shaking of the tube over a period of up to 15 min. This resulted in the separation of an oil and a water phase. After the separation of the two phases 700 μL of GCDM was added and 900 μL of medium with the bacterial cells was transferred to a sterile tube. The number of bacteria in this solution was then determined using a Coulter Counter (Beckman-Coulter). Subsequently, the cells were diluted in GCDM to give a concentration of 2 x 10^5 cells per milliliter and a new emulsion was prepared as described. This process was repeated serially for up to 31 times. Throughout the experiments, stock solutions of cells from broken emulsions supplemented with 15% (vol/vol) glycerol were prepared and stored at −80 °C in regular intervals.

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Supporting Appendix

Availability of public goods shapes the evolution of competing metabolic strategies

Short title:
Growth in isolation favors increased efficiency

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SI Appendix: Text

Yield/rate trade-off

Well-described examples of a yield/rate trade-off are the ones dealing with metabolic shifts in central carbon metabolism. For instance the Crabtree effect in yeast describes that an increase of the growth rate leads to production of ethanol even in the presence of sufficiently high oxygen concentrations. Such a shift from respiration to fermentation causes large differences in ATP and biomass yield (32 mol ATP per glucose versus 2 mol ATP per glucose, respectively) (1). Other examples for such a trade-off are the shift from acetate production to lactate production in lactic acid bacteria (2), the production of acetate by *E. coli* (3) at high growth rates and also the Warburg effect in cancer cells (4). Although these examples demonstrate such a trade-off, several attempts to evolve organisms with an increased yield failed. Next to the examples mentioned in the main text, the yield/rate trade-off was studied in *E. coli* evolving in the laboratory for 20000 generations. In this study the authors did not find a trade-off when comparing evolved strains with their ancestors or across independently evolved populations (5). However, within three out of four evolved populations they did find a significant negative correlation between yield and rate. The authors speculate that the failure to observe a trade-off in the first two comparisons could be due to incomplete adaptation to the growth medium when they started the experiment or because the maximum possible growth rate was attained, which would hamper the detection of a yield-rate trade-off. The authors do acknowledge limitations of their experimental setup that possibly compromise the detection of such a trade-off, and suggest dedicated experiments for further investigation.

MacLean (6) compared the glucose uptake rate and the biomass yield of 13 different yeasts from the *Saccharomyces* clade (data obtained from Merico et al. (7)). After the omission of 2 strains that did not produce ethanol, a significant negative correlation was found between the glucose uptake rate and the biomass yield. However, when the actual growth rate measured in the same experiment is compared to the biomass yield, this correlation does not exist anymore (SI Appendix; Fig. S12). From an evolutionary perspective the growth rate is much more relevant to the yield-rate trade-off than the glucose uptake rate. The reason for this discrepancy between glucose uptake and growth rate might lie in the fact that most of these strains are not optimized for growth in the medium that this data was obtained in. Depending on how well a strain was adapted to the particular medium, the actual yield ratio could be far away from optimality, which makes it impossible to identify a yield/rate trade-off line.
Microbial growth in emulsion

In our study emulsions were generated by mechanically shaking growth medium with the appropriate cell density with suitable oil supplemented with a surfactant. The resulting emulsions droplets are polydisperse (droplets vary in diameter) and for our experiments we assumed an average droplet size of 50 µm (Figure S1). The size distribution of droplets did not change during at least three days of incubation, indicating that droplet fusion does not occur or is very limited. An average droplet size of 50 µm corresponds to a droplet volume of 65 picoliters. Based on the average droplet size, the prepared emulsions contained approximately 4.6 million droplets. As we used 300 µl of medium containing $2 \times 10^6$ cells per ml to prepare the emulsions the expected number of cells per droplet is approximately $(2 \times 10^6 \times 0.3)/4.6 \times 10^6 = 0.13$. Assuming that droplet occupation follows a Poisson distribution, it was calculated that 11.4% of all droplets were filled with a single cell and that less than 1% were occupied with more than one cell (Figure S1). Droplets with a smaller diameter have a smaller likelihood of being occupied by a cell and because the volume of a sphere scales with the third power of the radius smaller droplets form a relatively small fraction of the total volume. Bigger droplets are more likely to be occupied by more than one cell. Such droplets would not contribute to the selection of cells with an increased number of offspring if they co-reside in a droplet with a faster growing strain. This means that droplets with a large diameter will slow down the selection process but will not be detrimental to it. Based on an average droplet volume of 65 picoliters, an initial cells density of 1 cell per droplet and a maximum cell density of $1 \times 10^9$ cell/ml the number of cell divisions in a fully-grown droplet is approximately 6. 

*Lactococcus lactis* MG1363 can also form short chains of bacteria, which could lead to the inoculation of individual droplets with more than one cell. Since cells within a chain are likely to be genetically identical, this effect should not compromise the selection procedure.

To estimate the number or transfers in emulsion required to identify mutant strains we assumed that one in a million cells carries a mutation leading to an increased number of offspring. If the increase in the number of offspring is 30% the enrichment of this mutant will be more than three orders of magnitude within 30 transfers. If the increase in the number of offspring is 50% the enrichment after 30 transfers will be more than five orders of magnitude, which would render it making up more than 10 percent of the total population.

Serial propagation in emulsion allows selection for an increased number of offspring: Proof of principle

We used the protocol for serial propagation in emulsion to propagate *L. lactis*, a lactic acid bacterium that produces mainly lactate as a metabolic end product. In
*L. lactis* the production of acetate yields 50% more ATP compared to the production of lactate as a metabolic end product (Fig. 1). Consistent with a suggested yield/rate trade-off in organisms a lactate dehydrogenase (*ldh*) mutant, in which the glycolytic flux is mainly diverted towards acetate production, grows almost 4-fold slower but reaches 30% higher cell densities than the wild type strain (8). In a proof of principle assay we showed that in competition with the wild type strain the fraction of the slow but efficient *ldh* mutant increased if propagated in emulsion, while it rapidly decreased in suspension (Fig. 1).

**Serial propagation of *L. lactis* in emulsion selects for populations with an increased number of offspring**

In the main text we describe the selection of a high-yield mutant (HB60) through serial propagation in emulsion. However, a competition experiment of HB60 and the wild type strain MG1363 propagated in emulsion every second day resulted in the co-existence of the two strains but the fraction of HB60 did not increase. This was an unexpected result, as we selected HB60 using this same selection scheme. We hypothesized that the survival of HB60 in emulsion was lower than that of MG1363. Subsequent experiments revealed that variants with elevated final optical densities increased in frequency in the initial emulsion if the propagation was continued (Fig. 2) and that HB60 could invade the wild type population in emulsion when propagated every day, rather than every two days (SI Appendix; Fig. S3). These results corroborate the notion that the survival of HB60 compared to MG1363 in emulsion is compromised and that the initial EMS-mutagenized population contained no or very few wild type variants. The suggestion that very few or no wild type variants resided in the EMS-mutagenized population of MG1363 is further supported by two populations of EMS-treated MG1363 that were adapted in suspension for 120 generations. This is comparable to the number of generations during the 22 propagation steps in emulsion (~6 divisions per emulsion step). The suspension adapted populations MG1363_Sus1 and MG1363_Sus2 showed both a lower growth rate and yield than the wild type MG1363 (SI Appendix; Fig. S10).

**Full genome re-sequencing**

Full genome re-sequencing revealed that strain HB60 contained one point mutation in *ptnD* (see main text and Figs. S6, S8, S9) but also 3 loci where a mobile genetic element inserted into the genome. Transposable element IS981 inserted into either *i) the intergenic region between a hypothetical protein and the 50s ribosomal protein L10* *ii) into the coding region of a hypothetical protein and iii) in the intergenic region of two genes encoding hypothetical proteins* (Table S2). All three insertions were also found back in strains HB61 and HB62.
We cannot exclude that these insertions have an effect on the observed phenotype of HB60. However, the fact that in strains HB61 and HB62 three independent events led to the emergence of new promoters upstream of glucose transporters, indicate the importance of glucose transport for the selected phenotypes. It furthermore corroborates the importance of the identified mutation in the glucose transporter subunit ptnD in HB60. For its validation we tested a MG1363 derived strain in which the complete glucose transport system ptnABCD is deleted (NZ9000ΔptnABCD). This strain showed indeed a growth rate and growth yield similar to the one of HB60 (SI Appendix; Fig. S10). The serial propagation of NZ9000ΔptnABCD in suspension led to an increased growth rate and a decreased yield resembling the trajectories seen with the HB60 reversions towards HB61, HB62 and HB63.
SI Appendix: Tables

**Table S1:** Strains used in this study

<table>
<thead>
<tr>
<th>Strain</th>
<th>Description</th>
<th>Reference</th>
</tr>
</thead>
<tbody>
<tr>
<td>MG1363</td>
<td>L. lactis plasmid and phage cured derivative of NCDO712</td>
<td>Gasson 1983, Wegmann et al. 2007</td>
</tr>
<tr>
<td>NZ9000</td>
<td>pepC::nisRK derivative of L. lactis MG1363</td>
<td>Kuipers et al. 1997</td>
</tr>
<tr>
<td>NZ9010</td>
<td>ldh::ery derivative of L. lactis NZ9010; ldh negative strain that reverts to a Ldh positive phenotype through the activation of ldhB (Bongers et al. 2003)</td>
<td>Hoefnagel et al. 2002</td>
</tr>
<tr>
<td>NZ9020</td>
<td>ldh::ery; ldhB::tet derivative of L. lactis NZ89000; double mutant of ldh and ldhB in NZ9000</td>
<td>Bongers et al. 2003</td>
</tr>
<tr>
<td>NZ9000::ptnABCD</td>
<td>Derivative of NZ9000 containing a 1736-bp deletion in ptnABCD</td>
<td>Pool et al. 2006</td>
</tr>
<tr>
<td>NZ9000::ptnBA</td>
<td>Derivative of NZ9000 containing a deletion in ptnBA</td>
<td>Pool et al. 2006</td>
</tr>
<tr>
<td>HB60</td>
<td>MG1363 derivative selected after propagation in emulsion; shows a slow growth and high yield phenotype; carries a F65L mutation in ptnD</td>
<td>this study</td>
</tr>
<tr>
<td>HB61</td>
<td>HB60 derivative selected after propagation in suspension; shows a growth rate and growth yield phenotype similar to MG1363; carries IS905 upstream of the ptnABCD operon</td>
<td>this study</td>
</tr>
<tr>
<td>HB62</td>
<td>HB60 derivative selected after propagation in suspension; shows a growth rate and growth yield phenotype similar to MG1363</td>
<td>this study</td>
</tr>
<tr>
<td>HB63</td>
<td>HB60 derivative selected after propagation in suspension; shows a growth rate and growth yield phenotype similar to MG1363; carries IS905 upstream of the ptnABCD operon and IS905</td>
<td>this study</td>
</tr>
</tbody>
</table>

**Table S2:** Genome re-sequencing revealed three re-arrangements in HB60 and the additional insertions of IS905 upstream of ptnABCD and glcU in strains HB61 and HB63.

<table>
<thead>
<tr>
<th>Identified rearrangement</th>
<th>Insertion locus</th>
<th>Position of Insertion</th>
<th>Insertion length(bp)</th>
<th>detected in HB60</th>
<th>detected in HB61</th>
<th>detected in HB63</th>
</tr>
</thead>
<tbody>
<tr>
<td>ps435::IS905</td>
<td>intergenic</td>
<td>2690433</td>
<td>1310</td>
<td>yes</td>
<td>yes</td>
<td>yes</td>
</tr>
<tr>
<td>lmg_1205/rplC::IS981</td>
<td>intergenic</td>
<td>1175482</td>
<td>1231</td>
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<td>yes</td>
<td>yes</td>
</tr>
<tr>
<td>lmg1411::pseudo13::IS981</td>
<td>in coding region</td>
<td>1379183</td>
<td>2256</td>
<td>yes</td>
<td>yes</td>
<td>yes</td>
</tr>
<tr>
<td>ps507/ps506::IS981</td>
<td>intergenic</td>
<td>2221296</td>
<td>1228</td>
<td>yes</td>
<td>yes</td>
<td>yes</td>
</tr>
<tr>
<td>ptnAB/fer::IS905</td>
<td>intergenic</td>
<td>712501</td>
<td>1316</td>
<td>no</td>
<td>yes</td>
<td>yes</td>
</tr>
<tr>
<td>glcU/lmg_2562::IS905</td>
<td>intergenic</td>
<td>2521652</td>
<td>1326</td>
<td>no</td>
<td>no</td>
<td>yes</td>
</tr>
</tbody>
</table>

1 This rearrangement does not occur in the published genome of L. lactis MG1363 but it was found in the isolate that we started all experiments with (designated Gen0).

2 IS905 and IS981 occur 14 and 16 times in the genome of MG1363 respectively (Accession: NC_009004). Depending on the mapping of our reads with the different IS elements the insertion position and insertion length can vary by a number of bases.
SI Appendix: Figures

![Figure S1](image)

Emulsion droplets as prepared for the compartmentalized propagation of microbial cells (panel a). A histogram of the droplet diameters of 152 droplets from the picture in panel a (manually measured with ImageJ; http://imagej.nih.gov/ij/, 1997-2012) shows a mean droplet diameter of 43 µm (panel b), which equals a volume of 42 picoliter. Based on the average droplet size cell densities for droplet generation can be calculated. Droplet occupation will follow a probability distribution as shown in panel c (valid for a monodisperse emulsion (uniform droplet diameter)). Droplet size can slightly vary between different emulsions. Typically we saw the majority of droplet diameters ranging from 40-60 µm.
Growth curves (a) and cell size measurements (b) of strain HB60 (red) and MG1363 (black). The shaded areas indicate the SEM (n=12, panel a) (n=2, panel b). Please note that the emulsion based selection protocol selects for an increased number of viable offspring at the time of propagation and not necessarily for increased biomass yield. For instance a mutant with an increased number of viable offspring but decreased cell size and decreased total biomass would be favored by selection in emulsion. In the case of HB60 an increased number of offspring coincides with an increased biomass yield.
Invasion of the MG1363 wild type population by strain HB60. HB60 was mixed with MG1363 and propagated in emulsion every 24 hours. In the initial culture HB60 was not detected in 96 individual colonies (panel a). After 4 (panel b) and 8 transfers (panel c) in emulsion the fraction of HB60 increased as compared to the initial frequency in the population. The fraction of HB60 in the population is <1%, 6% and 23% in panel a, b and c respectively.
Figure S4

Organic acid profiles of strains MG1363 and HB60.
Organic acid profiles of HB60 (data points after 10 generations) and during its adaptation to growth in suspension for 50 and 90 generations. Three independent cultures were adapted in parallel (panels a, b and c) and from each culture a single colony was isolated and designated HB61, HB62 HB63 respectively. The organic acid profiles of the entire population after 90 generations resemble the profiles of the single colonies that were isolated.
Figure S6

Protein alignment of the protein family pfam03613, which encodes the PTS system mannose/fructose/sorbose family IID component (only the first 240 residues of the alignment are shown). The alignment shows the PtnD protein of MG1636 (top row) and the 20 most diverse members of the protein family as selected by the NCBI CDD database (retrieved on 24th September 2012). The alignment was made in ClustalW with standard settings and visualization was done in CLC sequence viewer. Amino acid conservation is indicated from blue to red with an increasing degree of conservation. At position 100 of the alignment a phenylalanine (F) residue is indicated to be well conserved. The G→T mutation that occurred at position 710325 (GenBank NC_009004) during the adaptation in emulsion lead to a change from phenylalanine at this position in MG1636 to a leucine in HB60 (F65L). The overall conservation of a phenylalanine residue in the mutated position in 3256 proteins (http://pfam.sanger.ac.uk; 24Sep2012) of this family is 86%. The IID component of the PTS systems is located in the cell membrane and together with component IIC it is responsible for the translocation of sugar moieties over the membrane. Based on the observed decrease of the glycolytic flux in HB60 (SI Appendix; Fig. S7) we conclude that the F65L mutation led to decreased PtnD activity.
Acidification rate normalized to wild type strain MG1363. Major metabolic end products in *L. lactis* are lactic acid, acetic acid and formic acid, which contribute to the acidification of the medium. The acidification rate is therefore a readout for the glycolytic flux. Compared to the wild type, strain HB60 shows 41% decreased acidification rate, while HB61, HB62 and HB63 show a 27%, 32% and 45% increase in their acidification rate respectively. HB60 shows a different organic acid profile, which might lead to an overestimation of the corresponding glycolytic flux based on the acidification rate.
The selection of MG1363 in emulsion resulted in the isolation of a mutant (HB60) with a point mutation (F65L) in ptnD. During the subsequent adaptation of HB60 in suspension insertion element IS905 (red) integrated into the
promoter region of the *ptnABCD* operon in strains HB61 and HB63. IS905 carries a perfect, outward facing -35 promoter element (underlined). This -35 element in combination with the down-stream located -10 element (underlined) closely resembles a consensus promoter sequence that did not occur in the parent strain. The original point mutation found in *ptnD* of strain HB60 remained in strains HB61 and HB63 during the adaptation in suspension. The up-regulation of transcription through the insertion of IS905 in promoter regions of MG1363 has been described before (9, 10). The insertion locus of IS905 is flanked by direct terminal repeats (light blue). The IS element is inserted at position 712501 in the genome of *L. lactis* MG1363 (GenBank NC_009004).

Panel b: In HB63 IS905 integrated also in the upstream region of the glucose permease gene *glcU*. Analogous to panel a this insertion resulted in the integration of the same -35 element (underlined) 17 bases upstream of a -10 element (underlined) which results in a region that closely resembles a consensus promoter sequence that did not occur in the parent strain. The IS element is inserted at position 2521652 in the genome of *L. lactis* MG1363 (GenBank NC_009004).
Figure S9

Genomic region of the *ptn* locus after the IS905 integration in strains HB61 and HB63. IS905 is indicated in red and the partial *ptnA* gene in green (panel a). Genomic region of the *glcU* locus after the IS905 integration in strain HB63. IS905 is indicated in red and the partial *glcU* gene in green (panel b). The IS element is flanked by inverted repeats (10) which are underlined and in bold.
Yield/rate plot of *L. lactis* MG1363 and 21 derivatives. HB60–S1, HB60–S2 and HB60–S3 are individual cultures of HB60 that were adapted to growth in suspension for 60, 100 and 160 generations (legend designations end with -P6, -P10 and -P160 respectively). Strains HB60–S1-P10, HB60–S2-P10, HB60–S3-P10 are single colony isolates from the individual cultures and they were designated HB61, HB62 and HB63 respectively. MG1363_Sus_1 and MG1363_Sus_2 are cultures of the originally EMS treated MG1363 culture that was propagated for 120 generations in suspension. Strains NZ9000_d_ptcBA (11) is deficient of the mannose PTS which was found to be mutated in HB60. Strain NZ9000_d_ptcBA (11) is deficient of a cellobiose PTS system that is also involved in glucose uptake in *L. lactis*. Strains NZ9000_d_ptnABCD and NZ9000_d_ptcBA were obtained on GM17 medium and adapted to growth in the chemically defined medium (CDMpc). The cultures indicated in this figure were adapted for 30, 40 and 100 generations (legend designations end with -P3, -P4 and -P10 respectively). Standard errors are shown (n=11). If error bars are not visible they fall within the plotted symbol. The diagonal line shows a linear regression line with an adjusted $R^2 = 0.71$ and a $p<0.0001$, DF=20. From the same cultures cell size, cell numbers, organic acid profiles and the total protein content was determined. See the correlations in Fig. 4 of the main text.
Figure S11

Serial propagation of the double ldh mutant NZ9020 for up to 280 generations did not result in an increased growth rate (primary y-axis) or a change in lactate production (secondary y-axis). NZ9020 was cultured for approximately 100 generations (culture designations ending with “-p10”) or approximately 280 generations (culture designations ending with “-p28”). The propagation for 100 generations was done for 96 individual cultures with similar results for growth rates. MG1363 is shown as a reference.
MacLean 2008 argued for the existence of a yield/rate trade-off based on the biomass/glucose uptake (qGluc) plot of different yeast species (bottom left panel). However, within the same dataset this correlation is not found if the growth rate is compared to either biomass yield or the glucose consumption rate, indicating that in yeasts there seems no clear correlation between growth rate and glucose uptake rate under these conditions as also observed by Youk et al. (13). Data taken from Merico et al. 2007 (7). Bottom panels show the individual data points fitted with a linear model (red line) and the top panels show the corresponding Pearson correlation coefficients and p-values.
SI Appendix: Materials and Methods

Chemically induced mutagenesis

For chemically induced mutagenesis, *L. lactis* MG1363 was grown in the presence of 25 mM ethyl methanesulfonate (EMS) overnight. This concentration of EMS allowed *L. lactis* to still grow exponentially, but at a decreased growth rate and to a lower final optical density. The exposure to EMS was stopped after 16 hours while the culture was still growing. EMS was removed by centrifugation of the culture, aspiration of the medium and re-suspending of the cells in GCDM to a final cell density of \( 2 \times 10^6 \) cells per ml. These cells were serially transferred in emulsion 31 times.

Surfactant synthesis

One mmol Krytox 157 FS-H (MW 7500), (DuPont) was stirred under argon or nitrogen, degassed with vacuum and refilled with argon or nitrogen 2-3 times to remove oxygen. Then 2mmol thionyl chloride (Sigma-Aldrich) were added dropwise to the reaction mixture while stirring for 5 minutes at 4ºC. Stirring was continued for another hour at room temperature. Then excess thionyl chloride was removed under vacuum for 30 minutes. During stirring 10 mL FC-3283 (3M, Novec) and 2 mmol 0,0′-Bis(2-aminopropyl) polypropylene glycol-block-polyethylene glycol-block-polypropylene glycol (MW 900) (Jeffamine ED-900; Sigma-Aldrich) were added drop-wise. The resulting emulsion was stirred for 2 hours at room temperature. Then 20 mL FC-3283 were added and the sample was filtered through celite. Finally FC-3283 was removed under vacuum. This surfactant was used without further purification. Although not used for the results presented here, we found that the use of 0.5% Pico-Surf™ (Dolomite Microfluidics) in HFE7500 (3M Novec) has similar emulsification properties as compared to the surfactant described above.

Proof of Principle experiment

Overnight cultures of strains NZ9000 and NZ9010 were inoculated at a ratio of 7:3 based on optical density measurements. This co-culture was serially propagated in suspension every 24 hours by preparing 1:1000 dilutions of 10 ml batch cultures. Another co-culture was propagated with the described emulsion based protocol every 48 hours for 4 transfers. Throughout the experiment dilutions of the culture were plated on GM17 or GM17 supplemented with 5 \( \mu \)g/ml erythromycin. NZ9010 is erythromycin resistant which allowed monitoring the fraction of NZ9010 in the mixed culture throughout the experiment.

Serial propagation in suspension

HB60 was serially propagated in 10 ml batch cultures by preparing 1:1000 dilutions every 24 hours. The fast growing revertants HB61, HB62 and HB63 are single colony isolates from three independent cultures that were propagated for
9 transfers. The number of generations generated throughout these propagations is approximately 90. Three cultures of NZ9020 were serially propagated in 10 ml cultures as described above for up to 280 generations. Additionally 96 cultures of NZ9020 were propagated in parallel by culturing them in deep-well plates that were filled with 1.8 ml medium. Every 24 hours cultures were propagated by inoculating a deep-well plate with a 96-pin replicator that transfers roughly 1-2 µl of the fully-grown culture. Ten transfers resulted in approximately 100 generations.

Growth curve analysis

The R software package was used to analyze the growth curves from microplate experiments. The optical density (OD) measurements were background corrected for each well by subtracting the average of the first 3 reads from all values. The OD after inoculation is below the detection limit of the plate reader, which allows it to use the first values as background measurements for individual wells. Individual background correction per well has the advantage that small variations caused by irregularities in the microplate or the medium volume will be taken into account. For the determination of the growth rate the region of exponential growth was determined as values that were above the noise level of the OD measurement and below 20-50% of the maximum OD reached by each curve. The slope of the ln-transformed data was calculated as the growth rate.

The maximum OD reached was determined as the average of the three highest OD values measured after cells go into stationary phase. Growth curves that were obvious outliers, which were usually caused by gas bubbles in wells were omitted from the analysis. Per 384 well plate (384 growth curves) we usually identified less than 3 of such outliers that were omitted from data analysis.

Dry weight, cell size and fermentation end products determination

Biomass dry weight of cultures was determined by filtering 4 ml of cell culture through a dried, and pre-weighed 0.2 µm pore filter using a vacuum pump and subsequent drying at 60°C until filters reached a stable weight. Bacterial cell size and number was determined in a Multisizer 3 (Beckman-Coulter), which was used with a 30 µm aperture according to the manufacturers instructions.

The extracellular concentration of glucose, lactate, formate, acetate, pyruvate, succinate and ethanol was quantified by HPLC analysis of fermentation supernatants obtained by filtration through a 0.2 µm polyethersulfone (PES) filter (VWR International B.V., Amsterdam, The Netherlands). Separation and quantification of the compounds of interest was achieved using an isocratic flow through an aminex ion-exclusion column using a previously described set up (14). The carbon flux towards lactate was estimated as the fraction of carbon [in mM] in the metabolic end-products lactate, acetate and formate: Fraction of lactate = (3×[lactate])/(3×[lactate] + 2×[acetate] + [formate]).
Acidification measurements

Cells were pre-cultured for 16 hours and propagated 1:20 in the same medium. When mid-logarithmic, cells were washed once in saline supplemented with 5µg/ml chloramphenicol and re-suspended in CDM medium that was diluted with four parts of saline and supplemented with 10 µM of 5-(6)-Carboxyfluorescein (#21877, Sigma-Aldrich) and 5 µg/ml chloramphenicol. Multiple wells of a black microplate with transparent bottom were filled with 190µl of the cell suspension and the optical density was determined. Subsequently 10 µl of 100mM glucose solution were added to each well (resulting in a concentration of 5 mM glucose) and fluorescence emission at 520 nm (Excitation 485 nm) was measured in regular intervals for 2 hours in a microplate reader (Fluorostar, BMG LABTECH GmbH, Ortenberg, Germany). This cell suspension was weakly buffered and allowed acidification measurements based on the decreasing fluorescence intensity of the pH-dependent indicator carboxy-fluoresceine. The addition of chloramphenicol prevents translation and therefore the measured acidification rate is a measure for the glycolytic flux with the protein machinery present during the growth phase in which cells were harvested. Acidification was plotted as the slope of the linear decrease in fluorescence corrected for the optical density (fluorescence in arbitrary units/minute/OD600) and normalized to strain MG1363.

Protein determination

To determine total protein content, 1000 µl of fully-grown cultures were washed two times with saline and re-suspended in 200 µl saline. 50 µl of 10% SDS were added and subsequently incubated at 90°C for one hour. Total protein was then determined by using the BCA protein assay Kit (Sigma-Aldrich) according to the manufacturers specifications. The 1000 µl of culture used were obtained by pooling 4 times 250 µl of independent cultures that were grown in a 96-well microplate in a plate reader.

Genome re-sequencing

Microbial DNA for genome sequencing was isolated from 3×10⁹ cells of an overnight culture with the DNeasy Blood & Tissue kit (Quiagen) according to the manufacturers instructions. Sequencing of genomic DNA was performed on an Illumina HiSeq2000 platform as described earlier (15), with the deviation that the enrichment step was omitted and the libraries were sequenced as single 101 bp reads. Sequencing resulted in 8834988, 20378452 and 9108362 reads for strains HB60, HB61 and HB63 respectively, which corresponds to an average sequence coverage of 318.9, 718.4 and 332 respectively. Sequence analysis was done with the Bresq Software package (16) using standard settings and the MG1363 genome as a reference (GenBank file: NC_009004). The call of mutations was based on comparison with the sequencing data obtained from the re-sequencing of the original strain that was used to start all experiments, designated L. lactis Gen0. The insertion of IS905 upstream of ptnABC and upstream of glcU was confirmed by PCR amplification and Sanger amplicon sequencing of the insertion loci.
The sequencing data of strains HB60, HB61 and HB63 is deposited in the NCBI Sequence Read Archive (SRA) under the project number SRP017852. The sequencing data of strain Gen0, is deposited under the accession number SRS385784.
SI Appendix: References


