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Understanding the solar-driven reduction of \( \text{CO}_2 \) on doped ceria†

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With the appropriate materials, one can construct redox cycles that use \( \text{CO}_2 \) as the oxidant, generating CO as the product. Here, we investigate thermochemical cycles using doped ceria compounds as the oxygen exchange medium. Doped samples are prepared using La, Cr, W, Zr, V, Y, and Ti as dopants. Studying the redox kinetics, we show that doping the pure ceria with zirconium strongly increases overall CO production, albeit at lower reaction rates. This is because the \( \text{CO}_2 \) reduction step is second-order with respect to \( \text{Ce}^{\text{III}} \). Doping the fluorite lattice with zirconium cations decreases the number of \( \text{Ce}^{\text{III}} \) ions at the surface, and consequently slows down the reaction. This result is counter-intuitive, since normally you would think that the more reduction, the better. But the reactivity towards \( \text{CO}_2 \) is actually determined by the surface \( \text{Ce}^{\text{III}} \) ions, and so migration of dopant ions on the surface reduces its reactivity, even though the bulk \( \text{Ce}^{\text{III}} \) concentration is higher. Our results demonstrate the importance of understanding surface kinetics when designing oxygen exchange materials for solar reactors.

Introduction

Energy demand and greenhouse gas emissions are two of the main problems that our society faces today. In principle, both can be solved by converting \( \text{CO}_2 \) to fuels using sunlight. Plants have been doing this for millions of years, albeit rather slowly. The challenge for us chemists is therefore finding ways for converting \( \text{CO}_2 \) to fuels more quickly and efficiently.¹

One of the most promising ways to meet this challenge is using solar-driven high-temperature thermochemical cycles based on metal oxide redox reactions. Such cycles can split water and \( \text{CO}_2 \), giving hydrogen and CO.²,⁴ This so-called synthetic gas mixture can then be converted catalytically to conventional liquid fuels, using for example Fischer–Tropsch technology.¹,⁵ Unlike direct thermolysis, these cycles avoid the \( \text{CO}/\text{H}_2/\text{O}_2 \) separation issues.

The problem is that the oxides used, typically \( \text{ZnO} \) and \( \text{SnO}_2 \), are volatile.⁶,⁷ They sublime during decomposition, requiring rapid quenching of gaseous products to avoid recombination. Similarly, less volatile oxides such as ferrite-based ones suffer from slow kinetics, sintering, plus yet some material loss due to volatilization.⁸

One class of materials that avoids these problems is non-stoichiometric cerium oxides (doped ceria compounds). These materials combine several advantages: (i) cerium, with the electron configuration \([\text{Xe}]^4d^5^6s^2\), has two stable valence states, \( \text{Ce}^{\text{III}} \) and \( \text{Ce}^{\text{IV}} \), that are suitable for redox cycling;⁹–¹¹ (ii) ceria crystallizes in the stable fluorite structure up to \( 2750 \) K,¹²,¹³ so they are unchanged over the entire reaction working range; (iii) the reduced and oxidised states have strikingly different colors (pale yellow and blue-black, respectively), so changes in the oxidation state are easily and visibly trackable;¹³ and (iv) doped ceria can accommodate high oxygen deficiencies by the substitution of elements on the cation sub-lattice. This gives high oxygen ion conductivities. Simultaneously, these materials can release significant levels of oxygen at low oxygen partial pressures and high temperatures. These two parameters are directly influenced by the type and amount of the dopant.¹⁴–¹⁹

That said, building efficient cycles using doped ceria is far from trivial. This is because efficiency is a combination of capacity (\( \text{CO} \) production per oxide mass) and speed (\( \text{CO} \) production per time). To reach high capacity at reasonable times, we must first understand and control the kinetics of this non-equilibrium system. Here we describe, for the first time, the factors governing the application of doped ceria as oxygen exchange reagents for thermocatalytic reduction of \( \text{CO}_2 \) to CO. To help readers who are unfamiliar with surface kinetics models we include also a short theory section.

Theory

The rate of a solid-state reaction is described by,²⁰–²⁴

\[
\frac{dx}{dt} = Ae^{-\left(\frac{E_a}{RT}\right)f(\alpha)}
\]

where \( A \) is the pre-exponential factor, \( E_a \) is the activation energy, \( T \) is absolute temperature, \( R \) is the gas constant, \( f(\alpha) \) is the
kinetic model, and $\alpha$ is the conversion. The kinetic parameters can be obtained from the isothermal kinetic data (Fig. 2) by applying eqn (1). Alternatively, eqn (1) can be transformed into a non-isothermal rate expression, describing the rate as a function of temperature at a constant heating rate,

$$\frac{\mathrm{d}a}{\mathrm{d}T} = \frac{\mathrm{d}a}{\mathrm{d}t} \frac{\mathrm{d}t}{\mathrm{d}T}$$

(2)

here $\mathrm{d}a/\mathrm{d}T$ is the non-isothermal reaction rate, $\mathrm{d}a/\mathrm{d}t$ is the isothermal reaction rate, and $\mathrm{d}T/\mathrm{d}t$ is the heating rate (denoted by $\beta$). Substituting eqn (1) into eqn (2) gives the differential form of the non-isothermal rate law:

$$\frac{\mathrm{d}a}{\mathrm{d}T} = A \frac{E_a}{\beta} e^{-\frac{E_a}{RT}} f(\alpha)$$

(3)

Separating variables and integrating eqn (1) and (3) gives the integral forms of the isothermal and non-isothermal rate laws, respectively, shown in eqn (4) and (5):

$$g(\alpha) = Ae^{\frac{E_a}{RT}} t$$

(4)

$$g(\alpha) = A \int_0^T e^{-\frac{E_a}{RT}} \mathrm{d}T$$

(5)

As eqn (5) has no analytical solution, we used the Coats-Redfern method to approximate the exponential integral by an asymptotic series expansion, giving eqn (6):

$$\ln \left( \frac{g(\alpha)}{T^2} \right) = \ln \left( \frac{AR}{\beta E_a} \left[ 1 - \frac{2RT_{\exp}}{E_a} \right]^{-\frac{E_a}{RT}} \right)$$

(6)

where $T_{\exp}$ is the mean experimental temperature. Plotting the left-hand side of eqn (6) versus $1/T$ gives the values of $E_a$ and $A$.

Table S1 in the ESI† (following the equations summarised by Khawam and Flanagan) shows the differential and the integral forms of the 17 different kinetics models used in this study. A short description of the model types is also included in the ESI†.

**Experimental section**

**Materials and instrumentation**

Chemicals were purchased from Sigma-Aldrich and used as received. Gases were purchased from Praxair and had a purity of 99.95% or higher. Thermogravimetric analysis was performed using a Netzsch TGA instrument with three individual mass-flow controllers coupled to a quadruple mass spectrometer (see Fig. 1).

**Catalyst preparation**

Catalysts were prepared using a modification of a previously published procedure, by co-melting a mixture of the metal nitrate hydrate precursors (chlorides or ammonium salts were used when nitrates were not available). After the precursor has liquefied, the pressure was lowered and a solid mixed-metal nitrate formed. This was converted into the mixed oxide by calcining in static air at 700 °C for 5 h. X-ray diffraction confirmed that all of the catalysts were monophasic, with a clear fluorite structure (see ESI for details†). Using the method described above, we prepared seven doped materials, using 10% wt La, Cr, W, Zr, V, Y, and Ti as dopants, as well as a sample with 30% wt Zr.

**General procedure for thermocatalytic redox cycling**

A blank experiment was run before every measurement, using an empty crucible to correct the mass signal. This ensures we are measuring the redox kinetics of ceria, which is not influenced by TGA response function. About 100 mg of material was weighed in a platinum crucible and placed on the thermobalance. Then, residual air in the TGA chamber was replaced with argon, to operate in inert atmosphere and improve the reduction yield by decreasing the oxygen partial pressure (Fig. 1). The sample was heated in an argon flow and the mass variation was registered continuously (this mass variation can be directly correlated to the oxygen release during the reduction step or to the re-oxidation of the material during the CO$_2$ splitting step).

In a typical experiment, five successive cycles (reduction and reoxidation) were done. The reduction step consisted of heating the sample to 1400 °C at 10 °C min$^{-1}$, and then maintaining this temperature for 1 h. The mass loss registered above 800 °C is directly correlated to the oxygen released from the oxide. Then, the temperature was lowered to 1100 °C for the second re-oxidation step, and CO$_2$ was injected into the furnace chamber, reacting with the oxygen-deficient material and producing CO.

The CO$_2$ stream was injected from the auxiliary gas inlet and mixed with argon, the carrier gas (total flow rate 100 mL min$^{-1}$; 50% CO$_2$). Table 1 summarizes the experiments done.

**Procedure for kinetic studies**

The above general procedure was modified as follows: (i) the reduction temperature was changed in between cycles ranging from 1000 °C to 1400 °C, while the oxidation step was kept constant at 1000 °C; (ii) the oxidation temperature was modified for the different cycles going from 1000 °C to 600 °C while the reduction temperature was kept at 1400 °C for all the cycles. The gas flows and concentrations were identical to those in the general procedure. Isothermal steps lasted for 1 h and the heating and cooling temperature was 10 °C min$^{-1}$. The mass changes are converted to the moles of O$_2$ released (reduction step) per gram of ceria or doped-ceria using eqn (7),

$$n_{O_2} = \frac{\Delta m_{\text{mass}}}{M_{O_2} m_{\text{ceria}}}$$

(7)

where $\Delta m_{\text{mass}}$ is the mass variation measured by TGA; $M_{O_2}$ is the molecular weight of O$_2$; and $m_{\text{ceria}}$ the mass of ceria used in the experiment.

The reduction level, %Ce(III) is then calculated using eqn (8),

$$\% \text{Ce(III)} = \frac{n_{O_2}}{n_{O_2,\text{max}}}$$(8)

Taking into account that

$$n_{O_2,\text{max}} = \frac{(1 - \delta)}{4M_{\text{ceria}}}$$

(9)
here, \( n_{O_{\text{max}}} \) is the maximum amount of oxygen (mol g\(^{-1}\)) that could be released if Ce(IV) was completely reduced to Ce(III), \( d \) is the stoichiometric coefficient of zirconium in Zr\(_x\)Ce\(_{1-x}\)O\(_2\) \((d = 0 \text{ for pure ceria})\), and \( M_{\text{ceria}} \) is the molecular weight of ceria depending on the Zr content. \%Ce(III) thus quantifies the percentage of Ce(III).

**Results and discussion**

Thermal reduction of doped ceria

From our previous work we know two important facts.\(^{16,17,19}\) First, that CeO\(_2\) can act as an oxygen exchange reagent for reducing CO\(_2\). Second, that we can change the rate and magnitude of the oxygen migration to and from the lattice by doping the pure ceria with up to 10–15% metal ions of similar charge and/or radius to those of Ce(IV), while keeping the fluorite lattice intact.\(^{2–4,27,28}\) We thus tested first a series of Ce\(_{0.9}M_{0.1}\)O\(_2\) \((M = \text{Zr, Y, V, Cr, W, La, Ti}; \text{see ESI for details}^\text{\dagger})\). Of these, only zirconium-doped ceria showed a significant increase of CO production. We focused therefore on this material. Fig. 2, top, shows a typical multi-cycle profile. We see that upon thermal treatment in inert conditions the Ce(IV) is gradually reduced to Ce(III). If we then decrease the temperature down to 1100 °C and feed CO\(_2\), the Ce(III) ions are immediately oxidized, giving CO and Ce(IV)O (eqn (10)). This cycle can be repeated at least five times without any loss of activity.

\[
\text{CO}_2 + \text{Ce(III)} \xrightarrow{1100 \degree C} \text{CO} + \text{Ce(IV)O} \tag{10}
\]

Following this, we repeated the redox cycles, but this time running the oxidation step at five different temperatures, from 1000 °C down to 600 °C. Even at 600 °C, CO\(_2\) was reduced to CO, reflecting the large energy penalty paid during the Ce(IV) reduction step. We also confirmed the exothermicity of the total reaction of CO\(_2\) reduction plus Ce(III) oxidation using differential scanning calorimetry.\(^{4,29}\)

**Kinetic analysis**

Several studies reported CO\(_2\) reduction using ceria-doped materials.\(^{2–4,27,28}\) Most of these focus on the reduction step, aiming at high degrees of reduction. While this is an important goal, it must be matched with a high reaction rate. This is

<table>
<thead>
<tr>
<th>Sample</th>
<th>Temperature of reduction, °C</th>
<th>Temperature of oxidation, °C</th>
<th>Number of cycles</th>
</tr>
</thead>
<tbody>
<tr>
<td>CeO(_2)</td>
<td>1400</td>
<td>1100</td>
<td>5</td>
</tr>
<tr>
<td>Ce(<em>{0.9}M</em>{0.1})O(_2), M = Zr, Y, V, Cr, W, La, Ti</td>
<td>1400</td>
<td>1100</td>
<td>5</td>
</tr>
<tr>
<td>CeO(_2)</td>
<td>1400</td>
<td>1000, 900, 800, 700, 600</td>
<td>5</td>
</tr>
<tr>
<td>Ce(<em>{0.8}Zr</em>{0.2})O(_2)</td>
<td>1400</td>
<td>1000, 900, 800, 700, 600</td>
<td>5</td>
</tr>
<tr>
<td>CeO(_2)</td>
<td>1000, 1100, 1200, 1300, 1400</td>
<td>1000</td>
<td>5</td>
</tr>
<tr>
<td>Ce(<em>{0.8}Zr</em>{0.2})O(_2)</td>
<td>1000, 1100, 1200, 1300, 1400</td>
<td>1000</td>
<td>5</td>
</tr>
</tbody>
</table>

Fig. 1 Schematic representation of the experimental set-up.
especially important for practical applications using solar energy, where continuous operation is preferable. The best way to work continuously is using a cylindrical rotor coated by a reactive oxide with two reaction zones, one for releasing oxygen and the other for reacting CO₂ (see schematic in Fig. 3). Both reactions should have comparable rates for efficient continuous redox cycling.

To understand the reaction profiles shown in Fig. 2, we include also the derivation of the kinetic parameters of the ceria reduction and oxidation steps. We derived these from the thermogravimetric analysis at isothermal and non-isothermal conditions (see the Theory section).

Kinetics of ceria and doped ceria reduction

We then fitted the experimental results to the most plausible kinetic models for solid-state reactions (17 models in total, details in the ESI†). Analysing the dynamic step (the ceria reduction step) we see that no single model fits the entire data set. Rather, we see two slopes. Fig. 4 shows, as an example, the Arrhenius plots for ceria and Ce₀.₉Zr₀.₁O₂ following Jander’s diffusion model (D3 model). Although this model gives the best linear fit, it still deviates from the data at low temperatures (below ca. 900 °C). This is because the activation energy changes as the temperature increases. In other words: there are two different mechanisms involved.

The reduction of the lattice includes: (i) oxygen diffusion through the surface in the form of O²⁻; (ii) diffusion in grain and across grain boundaries in the form of oxygen ions. We can then consider two different situations: at low temperatures, the concentration of oxygen in the lattice is high, and oxygen diffusion through the grain boundaries is maximized. Consequently, the rate-limiting step is the oxygen generation at the surface. Conversely, at high temperatures we have less oxygen in the lattice and the diffusion of this oxygen becomes the rate-limiting step. Indeed, the D3 model fits well because it assumes that the reaction at the surface is fast. Thus, the reduction rate is controlled by diffusion of the oxygen ions through the boundary layers.

We can calculate the activation energy for both mechanisms. The activation energy at low temperature is approximately half of that calculated at higher temperatures, ~100 kJ mol⁻¹ for pure ceria. These results agree with those published by Lai et al. for the given range of temperatures (1000–600 °C). Thus, we focus also on the activation energy for the high-temperature step. The pure ceria sample has a higher $E_a$ value (235 kJ mol⁻¹) than Ce₀.₉Zr₀.₁O₂ (162 kJ mol⁻¹). This tells us that the reduction...
is faster in the doped ceria. Lower activation energy of Ce0.9Zr0.1O2 is in line with its higher capacity for CO production.

To further check those two mechanisms, we ran another experiment where the metal oxide was reduced isothermally at different temperatures. Fig. 5 shows the temperature profile and the result for Ce0.9Zr0.1O2. Here the samples are heated up to a given temperature and left for one hour. Thus, we can analyze how fast the oxygen is released at the desired temperature. After that, the sample is cooled down to 1000 °C and oxidized with CO2.

These results were fitted using eqn (4) for all 17 kinetic models. Analysing these fits for Ce0.9Zr0.1O2, we found that at low temperature (1000 °C) the experimental results fit the area-contracting model (R3)33–38,41 reflecting the sintering of the crystals and reduction of the reactive surface area. The XRD and N2 adsorption isotherms (see ESI†) of the samples after the redox cycles indicate that the crystal size is very large (Ce0.9Zr0.1O2 655 nm and CeO2 581 nm). This means that the surface to volume ratio of the crystal is low and consequently the process at low temperatures (surface reduction) reach low values of conversion. However, above 1200 °C, the results fit to 3D diffusion models (D3). This is also in agreement with the non-isothermal results. The pure ceria sample was inactive below 1200 °C. At high temperatures the results fit to D3 models.

From these experiments, we conclude that both Ce0.9Zr0.1O2 and pure ceria are reduced following two mechanisms: below 1100 °C, only the surface is reduced, while at higher temperature the rate-limiting step is the diffusion of oxygen anions through the lattice to the surface.

**Kinetics of ceria and doped ceria oxidation**

Using the same set of experiments, we now studied the oxidation kinetics (i.e., the reduction of CO2) for the doped ceria. Here, all the analyses pertain to isothermal conditions. The black curve on the bottom graph of Fig. 2 gives information on the effect of the temperature in the oxidation of ceria. Similarly the black curve on the bottom of Fig. 5 gives information on the effect of initial Ce(III) concentration (since the ceria material is reduced at different temperatures, producing five initial Ce(III) concentrations).

Fitting the oxidation profile of ceria after reduction at 1400 °C to the 17 kinetic schemes included in the ESI,† we saw that the only acceptable scheme was that of a second-order reaction. This fits with the surface reaction (Scheme 1), where two electrons reduce the carbon from C(iv) to C(ii).

This can be considered as second-order kinetics with respect to the Ce(III) concentration, since we used an excess of CO2. The reaction profile does not change above 700 °C (see Fig. 6). At such high temperatures the reaction rate constant, which shows Arrhenius behavior, is less influenced by the temperature. Mass transport limitations were excluded since experiments performed for pure ceria and doped ceria compounds (Fig. 6 and 8) were run in identical conditions having very similar particle size. Any mass-transport or heat-transport limitation would result in identical profiles. The fact that the profiles differ confirms that there is no mass/heat transfer limitation under these conditions.

The second-order kinetics with respect to Ce(III) means that the reaction is highly sensitive to the Ce(III) concentration. We therefore ran additional experiments using different initial Ce(III) concentrations. Fig. 5 shows the temperature profile (blue stepped graph, top) as well as the degree of reduction (black curve, bottom). After every treatment in inert conditions the sample was cooled down to 1000 °C and oxidized using CO2. We then analysed oxidation step at 1000 °C. Fig. 7 shows how the relative Ce(III) concentration decreases vs. time for different

\[
\text{CO}_2(g) + 2\text{Ce}^{\text{III}} + V_0^{\text{O}} \rightarrow \text{CO}(g) + 2\text{Ce}^{\text{IV}} + O_0^{\text{X}}
\]

Scheme 1 Kroger–Vink notation for the reduction of CO2 by ceria. In this notation CeCe is a small polaron (free electron) and V0 is an oxygen vacancy.12

![Fig. 5](image) CO/CO2 redox cycling at increasing reduction temperatures, from 1000 to 1400 °C, while the oxidation temperature is kept at 1000 °C, for the sample Ce0.9Zr0.1O2. The blue line gives the temperature program, while the black line shows the Ce(III) concentration profile.

![Fig. 6](image) Ce(III) concentration during the Ce0.9Zr0.1O2 oxidation at five different temperatures. The sample was previously reduced at 1400 °C.
initial concentrations. We see a strong influence of the initial concentration in the kinetics. The more Ce(III) is present at the beginning of the oxidation, the higher the reaction rate. These curves also correspond to second-order kinetics, with an oxidation rate constant of 0.043 min$^{-1}$ Ce(III)/C$_0$.

Thus, our kinetics analysis of the Ce$_{0.9}$Zr$_{0.1}$O$_2$ oxidation suggests that CO$_2$ first approaches the highly reactive reduced Ce$_{0.9}$Zr$_{0.1}$O$_2$ surface, and then reacts in a two-electron process, oxidizing two Ce(III) ions to Ce(IV). The oxygen anion easily diffuses into the lattice, "cleaning up" the surface that can then react again with another CO$_2$ molecule.

We then ran the same analysis using the pure ceria sample. Again, we found second-order kinetics. Furthermore, the oxidation rate was constant when we change the temperature range (cf. the curves in Fig. 6 and 8). This indicates that the apparent activation energy is even lower than that of Zr-doped ceria.

Note that in the case of pure ceria the oxidation was faster, despite its lower initial concentration of Ce(III). We kept the same scale for Fig. 6 and 8 for ease of comparison. This may seem counter-intuitive, but bear in mind that though Ce$_{0.9}$Zr$_{0.1}$O$_2$ has higher reduction capacity as a whole, the reaction takes place at the surface, which is diluted with a minimum of 10% with Zr (the real value will be even higher because of Zr segregation to the surface, as shown by Bueno and co-workers).

To validate this, we ran another experiment with Ce$_{0.7}$Zr$_{0.3}$O$_2$ (see Fig. 9). We see that the reduction capacity strongly increases with the doping, but the regeneration is very slow. In fact, when the temperature of oxidation decreases below 900 °C, the sample does not fully oxidize within 1 h. This experiment shows that doping should be used cautiously to avoid adverse effects.

Finally, analysing the pure ceria sample for initial concentration effects gave similar results to those of Ce$_{0.9}$Zr$_{0.1}$O$_2$. The reaction rate was strongly dependent on the initial Ce(III) concentration, and followed second-order kinetics. The rate constant was an order of magnitude higher than that found for Ce$_{0.9}$Zr$_{0.1}$O$_2$, affirming that the Ce(III) concentration at the surface is higher for pure ceria.

These results show that by choosing the right amount of dopant, one can balance the reduction and oxidation rate, thus maximizing the performance of the rotatory reactor. For example, samples with high dopant loadings are difficult to oxidize, due to their slow kinetics. Conversely, samples with low loading (10% wt) perform better.

**Conclusion**

Our studies show that the oxidation of Ce(III) follows second-order kinetics, where two electrons are recombined for every CO$_2$ molecule. This process depends on the Ce(III) concentration at the surface. In principle, doping ceria with zirconia is beneficial. The activation energy of reduction is significantly lower for the doped samples than for the pure ceria sample. But the Ce(III) oxidation rate of the doped sample is slower than that of pure ceria, because there are fewer Ce(III) ions available at the doped oxide's surface. The dopant acts as a diluent at the surface of the sample decreasing therefore the concentration of Ce(III) at the surface. Thus, doping has both advantages and
limitations, and should be applied carefully if one wants to maximise the efficiency of thermocatalytic cycles for practical energy conversion purposes.

Nomenclature

<table>
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<th>Symbol</th>
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<td>$T$</td>
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<tr>
<td>$\alpha$</td>
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</tr>
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<td>$\beta$</td>
<td>K min$^{-1}$</td>
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<tr>
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<td>J mol$^{-1}$</td>
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<tr>
<td>$R$</td>
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<tr>
<td>$A$</td>
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<tr>
<td>$k$</td>
<td>Units depend on kinetic model</td>
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<tr>
<td>$T_{exp}$</td>
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Acknowledgements

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