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A Self-Assembled Molecular Cage for Substrate-Selective Epoxidation Reactions in Aqueous Media

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ABSTRACT: Encapsulation of a manganese porphyrin in a self-assembled molecular cage allows catalytic epoxidation of various substrates in 1:1 water/acetonitrile mixtures. The cage acts as a phase-transfer catalyst and creates a protective environment for the catalyst improving the stability. The encapsulated catalyst also allows discrimination between styrene derivatives of various sizes. In a direct competition experiment, the selectivity of the epoxidation reaction could be inverted with respect to a benchmark catalyst.

KEYWORDS: manganese, porphyrin, epoxidation, size-selective, supramolecular chemistry

INTRODUCTION

Metallo-porphyrins are widely applied as synthetic models for Cytochrome P-450 enzymes. Over the last decades, many systems have been reported describing both functional and structural analogues of this important class of natural catalysts. The major drawback of most of these mimics is the fast deactivation of the catalyst due to two commonly encountered deactivation pathways. The formation of μ-O-bridged dimers results in a significant decrease in the reaction rate, whereas ligand oxidation can result in complete loss of activity over time. Several elegant approaches have been used to circumvent these problems by tuning of the electronics. For example, halogenated porphyrins suffer much less from deactivation via dimer formation. In natural enzymes, such decomposition pathways are prevented by hosting the active site in a protective cavity of the protein matrix. As such, “picket-fence” porphyrins have been developed in a bioinspired approach to protect the catalysts by increasing the steric bulk around the porphyrin ring. Most of these systems are, however, not water-soluble or do not provide full cage-encapsulation of the catalyst. In addition, the size of the catalytic pocket is often greatly reduced, resulting in hindered substrate access to the active site. Self-assembled supramolecular architectures have been used to improve the lifetime of the catalyst, thereby increasing the turnover numbers (TONs) of the manganese porphyrin oxidation systems. Recently, encapsulation of catalysts in supramolecular containers have been described, resulting in an improved activity or selectivity compared to the free catalyst. Transition-metal-catalyzed transformations with these capsules in aqueous media remains challenging. The use of aqueous media could create a driving force for organic substrate encapsulation and therefore lead to enhanced activity and substrate selectivity. We were therefore interested whether this approach would be viable in the epoxidation of alkenes in aqueous media to yield a more active and selective catalyst.

RESULTS AND DISCUSSION

We previously reported the synthesis and application of a molecular cage in polar reaction media. The large 16+ charged molecular cage was obtained by self-assembly from the corresponding building blocks (Scheme 1, top). The pores of the capsule allow substrates to enter the molecular cage to reach the encapsulated catalyst. By using a similar procedure as previously reported for the encapsulation of cobalt and zinc porphyrins (2-M) in cage 1, we now report the encapsulation of manganese chloride tetrapyridylporphyrin (Mn(TPyP) (Cl), 2-MnCl) (Scheme 1, bottom). The supramolecular cage 2-MnCl@1 was characterized by ESI-MS (see Supporting Information for mass analysis) and NMR.

The manganese porphyrin 2-MnCl is paramagnetic, which results in broadening of the 1H NMR cage signals after encapsulation (Figure 1b). Nevertheless, desymmetrization
was observed showing several signals which were also observed for the previously reported encapsulated zinc tetrapyridylporphyrin (ZnTPyP, 2-Zn), as depicted in Figure 1c.18 It should be noted that these signals do not correspond to chemical shifts commonly observed for manganese porphyrins, and the signals are therefore ascribed to cage signals, which show reduced symmetry upon encapsulation of the guest. The upfield shifted signal (6.3 ppm) assigned to the zinc porphyrin guest (2-Zn) in Figure 1c could not be observed for the manganese porphyrin 2-MnCl@1 in Figure 1b due to its paramagnetic nature. We investigated the catalytic activity of 2-MnCl@1 in the epoxidation of styrene (3, Scheme 2). Iodosylbenzene is often employed as the oxidant in manganese-catalyzed epoxidation reactions but is not commercially available and can disproportionate to explosive iodylbenzene (PhI=O) upon heating or prolonged storage.5

Figure 1. 1H NMR spectra (acetone-d6) of (a) empty supramolecular cage 1, (b) encapsulated manganese porphyrin 2-MnCl@1, and (c) encapsulated zinc porphyrin 2-Zn@1.

Scheme 2. Presumed Intermediates/Transition States Explaining Formation of Epoxide Product 4 (Stepwise and Concerted) and Aldehyde Product 5 (1,2-Hydrogen-Shift from the Radical Intermediate).20

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Therefore, we decided to use (diacetoxyiodo)benzene, a stable precursor to iodosylbenzene, as the oxidant in our studies.\textsuperscript{19}

Initial experiments showed a low activity of the supramolecular catalyst 2-MnCl\textsubscript{2}@1 in acetonitrile after 20 min (Table 1, entry 1). However, the activity was greatly increased by changing the solvent composition to a 1:1 mixture of acetonitrile and water (Table 1, entry 2). It should be noted that such large amounts of water have previously been reported to have a negative effect on the activity of similar catalytic systems.\textsuperscript{19} The selectivity also changed to yield the epoxide 4 and aldehyde product 5 in a 2:1 ratio. The more polar solvent employed might facilitate the 1,2-hydrogen shift to yield the aldehyde product. Furthermore, water could be involved directly in facilitating the 1,2-hydrogen shift.

It can be expected that the addition of water to the solvent system allows significantly faster in situ formation of iodosylbenzene from the used precursor leading to a higher active oxidant concentration.\textsuperscript{21,22} Indeed the use of iodosylbenzene as the oxidant. The catalyst is poorly soluble in the used solvent system. Yield = TON/TON\textsubscript{max} × 100% = TON/600 × 100%.

Table 1. Styrene Epoxidation Using Various Catalysts\textsuperscript{4}

<table>
<thead>
<tr>
<th>entry</th>
<th>solvent\textsuperscript{a}</th>
<th>catalyst</th>
<th>4 (TON)\textsuperscript{e}</th>
<th>5 (TON)\textsuperscript{e}</th>
<th>ratio 4:5</th>
</tr>
</thead>
<tbody>
<tr>
<td>1</td>
<td>MeCN</td>
<td>2-MnCl\textsubscript{2}@1</td>
<td>11</td>
<td>1</td>
<td>92.8</td>
</tr>
<tr>
<td>2</td>
<td>MeCN:H\textsubscript{2}O</td>
<td>2-MnCl\textsubscript{2}@1</td>
<td>187</td>
<td>86</td>
<td>68:32</td>
</tr>
<tr>
<td>3\textsuperscript{d}</td>
<td>MeCN</td>
<td>2-MnCl\textsubscript{2}@1</td>
<td>98</td>
<td>33</td>
<td>75:25</td>
</tr>
<tr>
<td>4\textsuperscript{d}</td>
<td>MeCN:H\textsubscript{2}O</td>
<td>2-MnCl\textsubscript{2}@1</td>
<td>235</td>
<td>99</td>
<td>70:30</td>
</tr>
<tr>
<td>5</td>
<td>MeCN:H\textsubscript{2}O MnTPP (6)\textsuperscript{d}</td>
<td>16</td>
<td>6</td>
<td>71:29</td>
<td></td>
</tr>
<tr>
<td>6</td>
<td>MeCN:H\textsubscript{2}O MnTPPS (7)</td>
<td>10</td>
<td>2</td>
<td>81:19</td>
<td></td>
</tr>
<tr>
<td>7</td>
<td>MeCN:H\textsubscript{2}O</td>
<td>2-MnCl\textsuperscript{d}</td>
<td>1</td>
<td>2</td>
<td>33:67</td>
</tr>
<tr>
<td>8</td>
<td>MeCN:H\textsubscript{2}O</td>
<td>2-MnCl\textsuperscript{d}</td>
<td>99</td>
<td>48</td>
<td>67:33</td>
</tr>
</tbody>
</table>

\textsuperscript{4}Reaction conditions: styrene (0.3 mmol), catalyst (0.5 μmol), solvent (2 mL), and iodobenzene diacetate (0.39 mmol) were stirred for 20 min under air. \textsuperscript{a}When multiple solvents are listed, a ratio of 1:1 was used. \textsuperscript{b}TON = turnover number, determined by \textsuperscript{1}H NMR with triphenylmethane as external standard. Depicted values are averaged over two runs. \textsuperscript{c}Iodosylbenzene was used as the oxidant. \textsuperscript{d}The catalyst is poorly soluble in the used solvent system. Yield = TON/TON\textsubscript{max} × 100% = TON/600 × 100%.

The increased activity of nonencapsulated 2-MnCl\textsubscript{2} compared to the free catalysts 6 and 7 is nonetheless interesting and can be ascribed partially to intermolecular pyridine coordination to manganese. It is well-known in the literature that additives such as acetonitrile and pyridine, for example, can significantly enhance the activity of homogenous cobalt porphyrin-catalyzed reactions.\textsuperscript{14} It is important to note that the activity of the caged catalyst 2-MnCl\textsubscript{2}@1 is substantially higher than that of nonencapsulated 2-MnCl. When we monitored the reaction in time for both caged catalyst 2-MnCl\textsubscript{2}@1 and free catalyst 2-MnCl, we observed that the cage does indeed stabilize the catalyst, resulting in a higher TON for the epoxide after 20 min (Figure 3).

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as pyridine\textsuperscript{23} or imidazole\textsuperscript{24,25} can increase the activity and stability of porphyrin-based epoxidation catalysts.\textsuperscript{26} It can be expected that the catalyst 2-MnCl has a pyridine ligand from an additional porphyrin molecule axially coordinated, thus influencing the electronic structure and thereby the reactivity.

Indeed, when catalyst 6 was studied in the presence of 4 equiv of pyridine, the TONs for products 4 and 5 increased significantly to 33 and 14, respectively, after 20 min of reaction. Furthermore, the self-aggregation of pyridine ligands to adjacent porphyrin molecules can be expected to create a protective site around the catalyst to further increase the TONs (Figure 4). This effect could also be achieved by addition of 4 equivalents of zinc tetraphenylporphyrin (ZnTPP) to the catalyst 2-MnCl to increase the total turnover number (see Supporting Information).

Next to improving the stability of the catalyst 2-MnCl by encapsulation, we were also interested in whether the selectivity can be influenced by cage 1. Previously, we reported the competition between substrates of variable size in cyclopropanation to observe a clear preference for the smaller substrates in the presence of the cage 1.\textsuperscript{18} The required entrance of the substrate through the pores of the molecular cage 1 likely slows down the reactivity of larger substrates. As such, we expect that 2-MnCl@1 could be used as a size-selective epoxidation catalyst.

We started our investigation by performing a direct competition experiment (Table 2) between styrene (3) and 4-benzhydrylstyrene (8) using 300 equiv of each of these substrates with respect to the catalyst.

We initially performed the reaction with control catalyst 6, which should not differentiate between the two substrates based on their respective size. We observed a ratio between the two products of 41:59 in favor of the more bulky epoxide 9 (Table 2, entry 1). Interestingly, applying our encapsulated catalyst 2-MnCl@1 for the same reaction resulted in a preference toward styrene, yielding the smaller and more bulky epoxide in a 65:35 ratio (Table 2, entry 2, TON = 204).\textsuperscript{34} To our surprise, the nonencapsulated catalyst 2-MnCl was even more selective for the smaller substrate (4:9 ratio = 79:21). It should however be noted that the activity for the 2-MnCl catalyst is also significantly lower compared to our encapsulated catalyst 2-MnCl@1. The nonencapsulated catalyst 2-MnCl most likely self-aggregates by coordination of the pyridine ligands to the manganese core of adjacent porphyrin molecules (Figure 4). This creates a steric confinement around the catalyst, thus explaining the observed size selectivity.\textsuperscript{35} This is also in agreement with the observed low TONs toward the bulky epoxides 9 and 10 in isolated experiments (TON = 16 and 14, respectively, see Scheme 3). The in situ-formed assembly likely has an even smaller cavity than the encapsulated catalyst 2-MnCl@1 as compared to 2-MnCl could be that the binding affinity of cage 1 is higher for the more bulky substrates (due to favorable phenyl-porphyrin interactions or the higher hydrophobic nature) than for styrene. Substrate binding in general is probably stronger in cage 1 than in the partial capsules.

<table>
<thead>
<tr>
<th>Entry</th>
<th>Catalyst</th>
<th>Ratio product 4:9</th>
<th>TON$^{[b]}$</th>
</tr>
</thead>
<tbody>
<tr>
<td>1</td>
<td>MnTPP 6</td>
<td>41:59</td>
<td>65</td>
</tr>
<tr>
<td>2</td>
<td>2-MnCl@1</td>
<td>65:35</td>
<td>192</td>
</tr>
<tr>
<td>3</td>
<td>2-MnCl</td>
<td>79:21</td>
<td>61</td>
</tr>
</tbody>
</table>

<table>
<thead>
<tr>
<th>Entry</th>
<th>Catalyst</th>
<th>Ratio product 4:10</th>
<th>TON$^{[b]}$</th>
</tr>
</thead>
<tbody>
<tr>
<td>4</td>
<td>MnTPP 6</td>
<td>40:60</td>
<td>41</td>
</tr>
<tr>
<td>5</td>
<td>2-MnCl@1</td>
<td>66:34</td>
<td>204</td>
</tr>
<tr>
<td>6</td>
<td>2-MnCl</td>
<td>77:23</td>
<td>67</td>
</tr>
</tbody>
</table>

$^{[a]}$Reaction conditions: styrene (0.3 mmol), bulky styrene or 11 (0.3 mmol), catalyst (0.5 μmol), solvent (2 mL), and iodosobenzene diacetate (0.3 mmol) were stirred for 20 min under air. $^{[b]}$TON = combined turnover number toward both epoxides, determined by $^1$H NMR with triphenylmethane or anisole as external standard. Depicted values are averaged over two experiments.

Figure 4. Schematic representations of porphyrin self-aggregation to form protective capsules.\textsuperscript{27}

Table 2. Competition Experiments for Size-Selective Catalysis

$^{[a]}$Reaction conditions: styrene (0.3 mmol), bulky styrene or 11 (0.3 mmol), catalyst (0.5 μmol), solvent (2 mL), and iodosobenzene diacetate (0.3 mmol) were stirred for 20 min under air. $^{[b]}$TON = combined turnover number toward both epoxides, determined by $^1$H NMR with triphenylmethane or anisole as external standard. Depicted values are averaged over two experiments.
constructed by self-assembly of 2-MnCl. Combined, this may well cause an offset in the size-selectivity caused by a slower diffusion rate of bigger substrates (and products) through the pores of cage 1.29

We continued to investigate the direct competition between styrene (3) and 3,5-di-tert-butylstyrene (11). As in the previous case, the control catalyst 6 showed preferred epoxidation of the bulky substrate 11 and a ratio of 40:60 was obtained (Table 2, entry 4). The encapsulated catalyst 2-MnCl@1 clearly favors styrene over the bulky substrate 11 (Table 2, entry 5; obtained ratio = 66:34), but the result is comparable to the previous competition experiment with styrene and 8. As it appears, the pores of the cage around 2-MnCl in the assembly 2-MnCl@1 are sufficiently large and flexible enough to allow both substrates to enter (partially) into the cavity, hereby leading to a clear but nonetheless moderate size-selectivity. Lastly, the most selective, though less active, system was once more obtained when 2-MnCl was used as the catalyst (Table 2, entry 6; ratio = 77:23, TON = 67). This shows once more that the self-assembly of 2-MnCl leads to smaller cavities around some remaining active manganese catalysts with an increased size-selectivity but lower activity.

To verify whether self-aggregation indeed results in the observed selectivity for the nonencapsulated catalyst 2-MnCl, we decided to vary the concentration of catalyst 2-MnCl. As expected, we observed a slight increase in the selectivity when a catalyst concentration of 1 mol % was used (ratio 4:10 = 82:18). Even more pronounced was the loss in selectivity when the catalyst concentration was decreased to 0.03 mol % (ratio 4:10 = 71:29). This effect of concentration was not observed for the encapsulated catalyst 2-MnCl@1. A catalyst concentration of 0.03 mol % resulted in a comparable product ratio of 68:32 in favor of styrene oxide 4. These results confirm that the size-selectivity observed in the competition experiments using the nonencapsulated catalyst 2-MnCl are indeed caused by self-aggregation.

To obtain further insight into which substrates would still be accessible by the encapsulated catalyst 2-MnCl@1 we decided to screen various substrates in the epoxidation reaction under the optimized conditions. For several alkenes used in this study, the kinetic diameter has been reported.30 The kinetic diameter varies from 5.5 Å for cis-cyclooctene to 7.8 Å for cis-stilbene. All substrates and products except for the very bulky substrates 4-benzhydroxystyrene 8 and 3,5-di-tert-butylstyrene 11 should therefore easily be able to pass through the pores of cage 1 (see Supporting Information). Hence, significant size-discrimination can only be expected when comparing the bulkiest substrates with smaller substrates.31 The results from our screening are summarized in Scheme 3. We found that the system is applicable for the epoxidation of various substituted styrene derivatives (Scheme 3, products 12 to 15). The system appears to be sensitive to small changes in the electronics.

Turnover numbers up to 258 toward the epoxide 12 were obtained, but no epoxide product 16 was formed in the oxidation of 4-methoxystyrene. Next, we examined the sensitivity of our systems toward substitutions on the alkene bond. The general reactivity trends of the various substrates 17 to 21 are in agreement with the activities reported previously for similar systems.32,33 Remarkably in the reaction of α-methylstyrene 21 large amounts of acetophenone were obtained (2 equiv with respect to the epoxide 21). Commonly this oxidative cleavage product is only observed after long reaction times in the presence of large amounts of the oxidant.34 The substrate scope was further expanded to aliphatic alkenes (Scheme 3, products 22 to 26), but the caged catalyst 2-MnCl@1 shows only poor reactivity in the epoxidation of both 1-decene and trans-4-octene (Scheme 3, products 22 and 23). Only trace amounts of the epoxides were detected (TON = 4 and 18 for products 22 and 23 respectively). The reactivity of 2-MnCl@1 toward a terminal alkene is lower than a comparable internal aliphatic alkene.35 When we used cis-4-octene as a substrate, a significantly higher reactivity toward the corresponding epoxide (Scheme 3, product 24 TON = 58) was obtained. No isomerization

“Significant amounts of the corresponding aldehyde product were observed. “Significant amounts of an oxidative cleavage product were observed. 2-MnCl was used as the catalyst for the TONs in brackets. Note: depicted TONs are toward the epoxide product and averaged over at least two runs.

Scheme 3. Epoxides Obtained after Reaction of the Corresponding Alkene under the Optimized Reaction Conditionsa,b,c

<table>
<thead>
<tr>
<th>Entry</th>
<th>TON</th>
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<tbody>
<tr>
<td>9</td>
<td>102 (16)</td>
</tr>
<tr>
<td>10</td>
<td>55 (14)</td>
</tr>
<tr>
<td>11</td>
<td>4</td>
</tr>
<tr>
<td>12</td>
<td>258</td>
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<tr>
<td>15</td>
<td>216</td>
</tr>
<tr>
<td>16</td>
<td>54(1)</td>
</tr>
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<td>17</td>
<td>33</td>
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<td>251</td>
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<td>25</td>
<td>101</td>
</tr>
<tr>
<td>26</td>
<td>81</td>
</tr>
</tbody>
</table>

aSignificant amounts of the corresponding aldehyde product were observed. 
bSignificant amounts of an oxidative cleavage product were observed. 

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toward the trans-epoxide product was observed in this reaction. Cyclic alkenes can also be used under the applied conditions showing a TON of 101 in the epoxidation of cis-cyclooctene (Scheme 3, product 25). Our system shows a decreased activity for the smaller cis-cyclohexene (Scheme 3, product 26, TON = 81), as commonly found for related systems. 33,36

As expected from the direct competition experiments, a decreased TON with respect to styrene for both product 9 (TON = 102) and 10 (TON = 50) was observed with our encapsulated catalyst 2-MnCl@1. Also the nonencapsulated catalyst 2-MnCl showed a very low activity for products 9 and 10 in isolated experiments (TON = 16 and 14, respectively). In general, the cage around the manganese catalyst seems to tolerate a wide range of differently substituted styrenes. However, apart from the above-mentioned size-selectivity, the pores of cubic cage 1 are likely too big to induce any further shape-selective effects between the substrates smaller than bulky styrene 8 and 11.

### CONCLUSIONS

In conclusion, we have shown that it is possible to encapsulate a manganese porphyrin catalyst in a cubic self-assembled molecular cage. The obtained catalyst is active in aqueous media for the epoxidation of a variety of alkenes to reach up to 319 turnover numbers toward the desired product. The surrounding cage functions as a phase-transfer catalyst and improves the stability of the encapsulated catalyst. Furthermore, the encapsulated catalysts show size-selectivity when mixtures of bulky and less bulky substrates are applied.

### EXPERIMENTAL SECTION

General conditions for the epoxidation reactions: Substrate (0.3 mmol) and catalyst (0.5 μmol) were mixed in a 10 mL vial, and solvent was added (2 mL). After addition of the oxidant (0.4 mmol), the mixture was stirred at 600 rpm for 20 min under air. Products were extracted with n-pentane (3 × 10 mL), dried over MgSO4, and filtered. Solvents were removed under reduced pressure (40 °C, 500 mbar). Triphenylmethane (60 μmol) was added as a reference, and the products were quantified by 1H NMR spectroscopy (CDCl3 was used as the solvent for analysis).

### ASSOCIATED CONTENT

#### Supporting Information

The Supporting Information is available free of charge on the ACS Publications website at DOI: 10.1021/acscatal.6b00283.

Rotatable model of the caged catalyst 2-MnCl@1 (PDB Synthesis and characterization data for 2-MnCl@1; detailed conditions and 1H NMR spectra for the performed reactions; an estimation of the pore size of 2-MnCl@1 (PDF)

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**Notes**

The authors declare no competing financial interest.

### ACKNOWLEDGMENTS

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